## **Can food save the fuel?:**

**Impact of protein co-production on microalgal biofuels** Soumyajit Sen Gupta, Sharad Bhartiya, Yogendra Shastri

**Department of Chemical Engineering, IIT Bombay** 

## **Motivation and Approach: Model features: Conclusions:** • Improve techno-economic feasibility <u>Only biodiesel</u> production cost = US \$16.3/L • Mass balance across the processes • Develop integrated biorefinery • Cost expressions for equipments • 16% reduction in cost due to protein co-• Multitude of alternatives and decisions • Objective: Minimize Net ALCC production • Use of model based optimization • Scheduling based on batch time • Cost distribution depends on desired • Flowsheet and design optimization • Scale-up for a realistic scenario product-mix

## **Biodiesel and Protein from microalgae: Processes and the superstructure**

	GROWTH	HARVESTING	DRYING	LIPID EXTRACTION	<b>TRANSESTERIFICATION</b> <b>REACTION</b>
		Technique		Solvent	
		• Settling		Solvent	
		Centrifugation		Chloroform-Methanol	
		Settling followed		(1:1 molar basis)	
		by contrifugation		• Methanol	Catalyst type
	Medium	by centrilugation		• Supercritical CO <sub>2</sub>	• Acidic $(H_2SO_4)$
	Cowdung	Stages of settling			• Alkaline (NaOH)
,	• Chicken waste	Primary		Duration	Catalyst quantity



• Number of ponds: 720 (10 ha each) microalgae

-	Harvesting of	0.397	• Technique: Settling with ACTIPOL	Gr	owth of microalgae	6.663	<ul> <li>Duration: 18 days</li> <li>Number of ponds: 1 728 (10 ha each)</li> </ul>
	cultivated solution Drying of	0.001	<ul> <li>FB1</li> <li>Flocculant amount: 2,643.7 kg/batch</li> <li>Number of settling tanks: 353 (2,500 m<sup>3</sup> each)</li> <li>0.001</li> <li>Solar drying</li> <li>12.455</li> <li>Solvent: Supercritical CO<sub>2</sub> at 600 bar; 5.9x10<sup>6</sup> kg/batch</li> <li>Duration: 3 h</li> <li>Number of extraction tanks: 72 (4,000 gallon each)</li> <li>0.633</li> <li>Reactant alcohol amount: 7,446.4 kg/batch</li> <li>Catalyst: Sodium Hydroxide; 6 wt % of reactant lipids</li> </ul>	Har	vesting of cultivated solution rying of harvested microalgae paste	1.241 <b>5.665</b>	<ul> <li>• Rumber of pollus: 1,728 (10 na cach)</li> <li>• Technique: Settling with ACTIPOL EM1</li> <li>• Flocculant amount: 5,098.8 kg/batch</li> <li>• Number of settling tanks: 255 (2,500 m<sup>3</sup> each)</li> <li>• Oven drying</li> </ul>
	Lipid extraction from dried biomass powder	action 12.455 ied owder		Lij dri	pid extraction from ed biomass powder	2.756	<ul> <li>Solvent: Chloroform and methanol (1:1 molar basis)</li> <li>Solvent amount: 4,980 L/batch</li> <li>Duration: 20 minutes</li> <li>Cell disruption technique: Microwave</li> <li>Number of extraction tanks: 3 (20,000 gallon each)</li> </ul>
Tr	Transesterification reaction of	0.633		T react	Transesterification tion of extracted lipid	0.629	<ul> <li>Reactant alcohol amount: 2,482.1 kg/batch</li> <li>Catalyst: Sodium Hydroxide; 6 wt % of reactant lipids</li> <li>Duration: 4 h ; Number of reactors: 2</li> </ul>
	extracted lipid			Ex	traction of protein	4.239	<ul> <li>Solvent requirement: 525.8 m<sup>3</sup>/batch</li> <li>Extraction vessel: 7 in number</li> </ul>
• Duration: 4 h; Number of reactors: 4				• The value obtained from the extracted protein was US \$ 7.467/L			

**Contact: Prof. Yogendra Shastri** (*yshastri@iitb.ac.in*)