

Optimization of bagasse utilization for ethanol production

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Introduction & Motivation



Availability of sugar processing waste

- Sugarcane processing gives bagasse as waste
- 1 Mg cane ➔ 280 kg bagasse.
- Bagasse presently used as boiler feed and fodder.
- More profitable uses of bagasse need to be explored

Production of second generation biofuels

- Renewable liquid transportation fuels becoming important.
- Second generation biofuels from non-food crops attractive.
- Should be cost competitive with conventional fuels
- Co-production a possibility

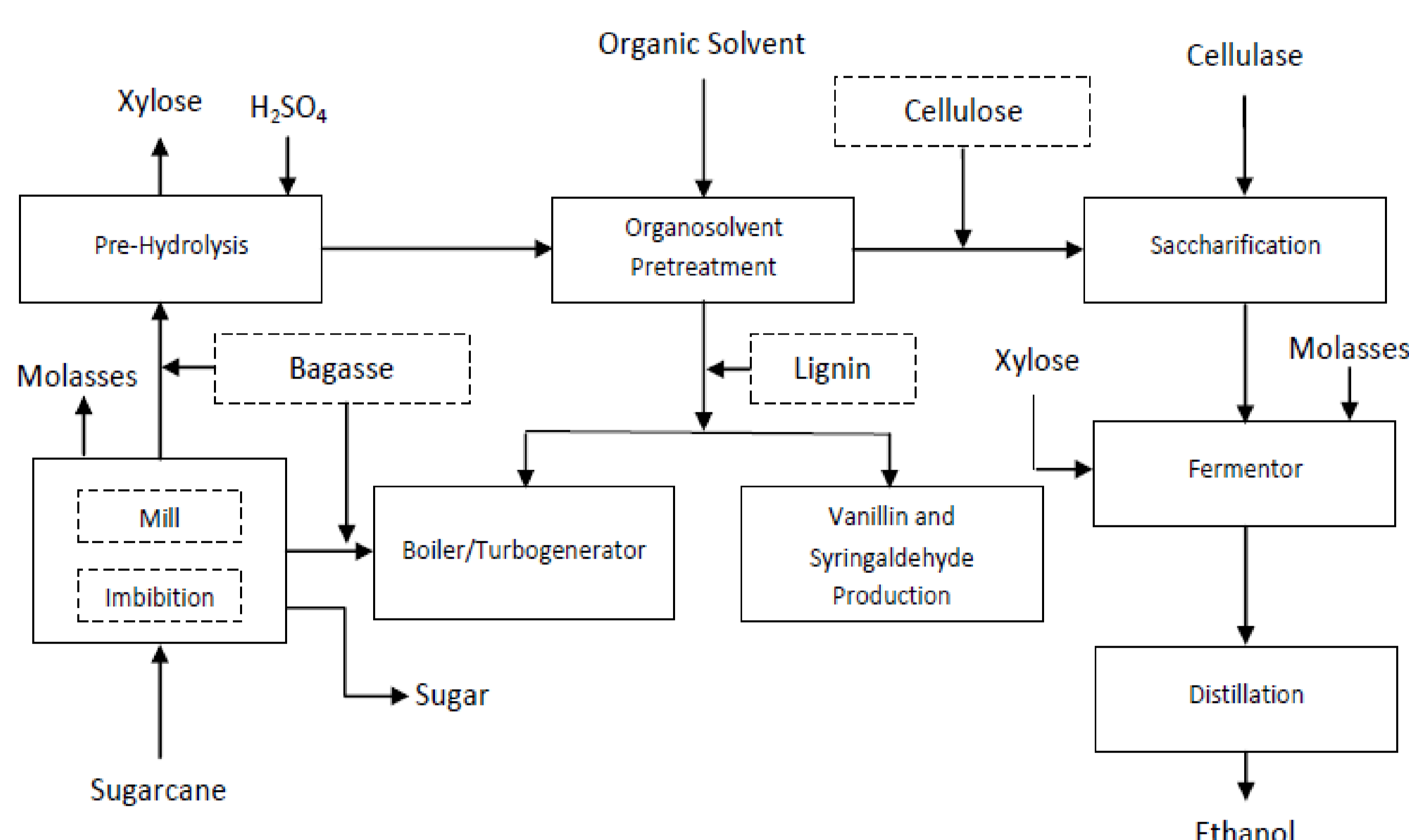
Objective

- Integrate bagasse to ethanol production in existing sugar mills
- Optimize the process synthesis for cost reduction
- Determine break even selling price (BESP) of ethanol
- Quantify impact of different factors on economic feasibility

Approach

- System level optimization model.
- Mass and Energy balances of processing units.
- Economics and equipment costing relationships.
- Maximization of overall profits.
- Inclusion of India specific data for India specific scenario.

Process Superstructure and Optimization Model Formulation



$$\text{Objective } \text{Max } z = \sum_i S.P_i \times x_i - \text{Total Cost}$$

where,

$S.P_i$ = Selling price of product i

x_i = Quantity of product i

Subjected to:

$$x_{Boiler}^{Bagasse} + x_{Ethanol}^{Bagasse} = F^{Bagasse}$$

$$C.P_{Bagasse} + C.P_{Lignin} + C.P_{Trash} \geq Q_1 + x_{Ethanol}^{Bagasse} \times Q_2$$

$$x_{Cost}^{H_2SO_4} = f_{Annual} \times F_{H_2SO_4} \times C_{H_2SO_4} \times x_{B2}^{H_2SO_4}$$

Key decision variables: $x_{Boiler}^{Bagasse}$ and $x_{Ethanol}^{Bagasse}$

BESP = Selling price of ethanol when $z = 0$

Model statistics:

No. of constraints: 110

No. of variables: 112

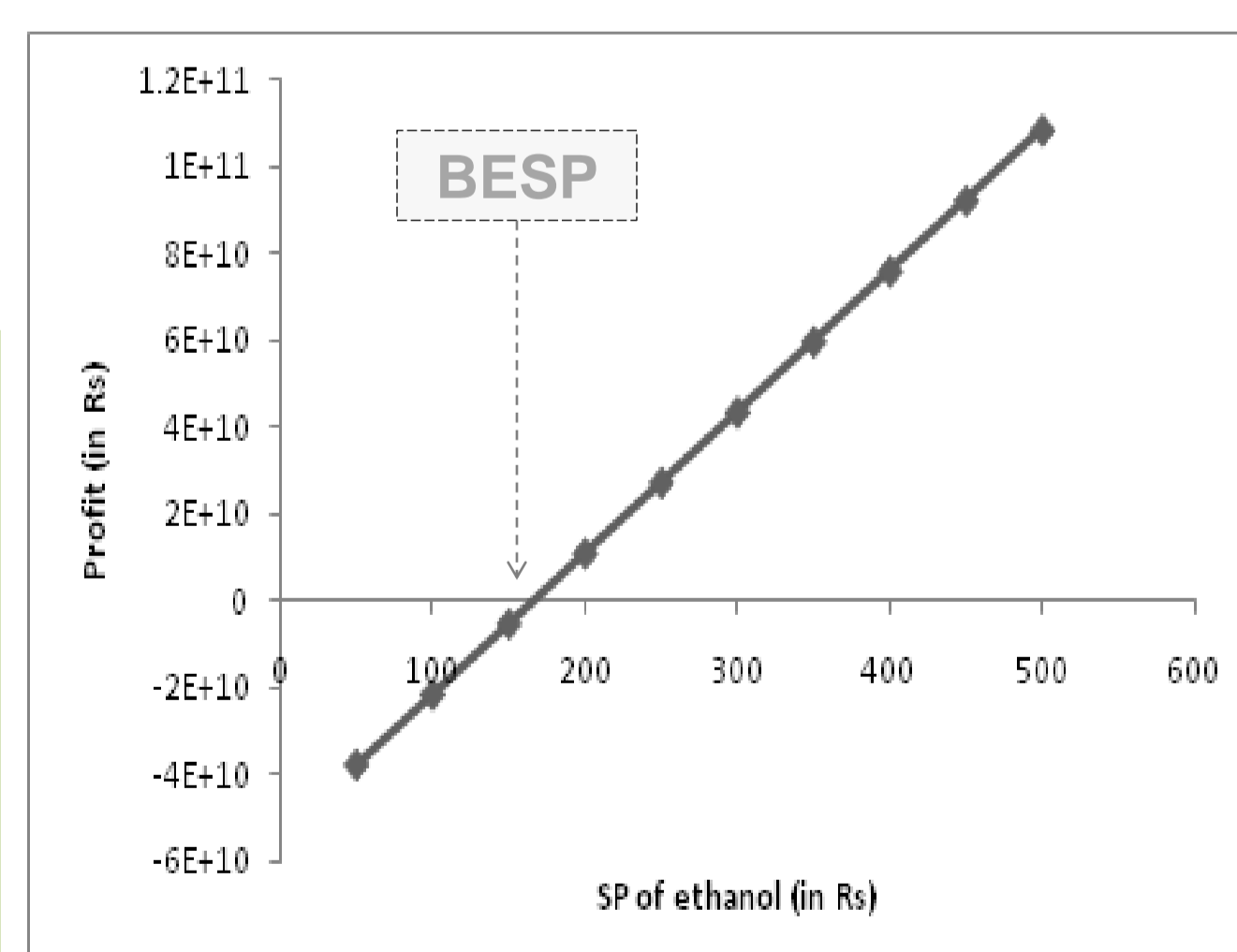
No. of discrete variables: 2

Case Study Application and Results

Case study and base case results

- 500 Mg/hr sugarcane feedstock
- Vanillin and syringaldehyde production are excluded

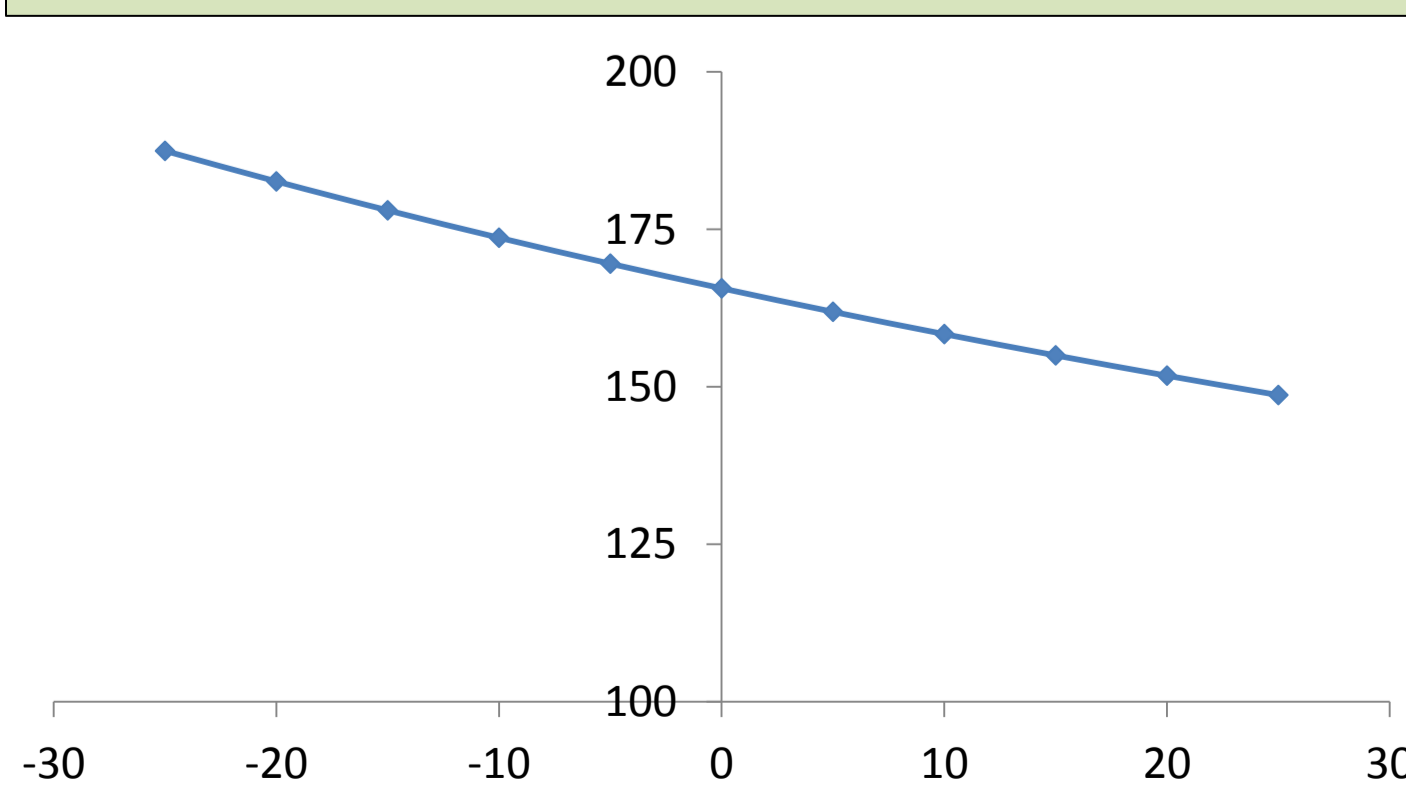
- Ethanol BESP was 165.65 Rs/litre.
- Allocation of 68.4 % bagasse for ethanol generation.
- All trash is utilized as energy source



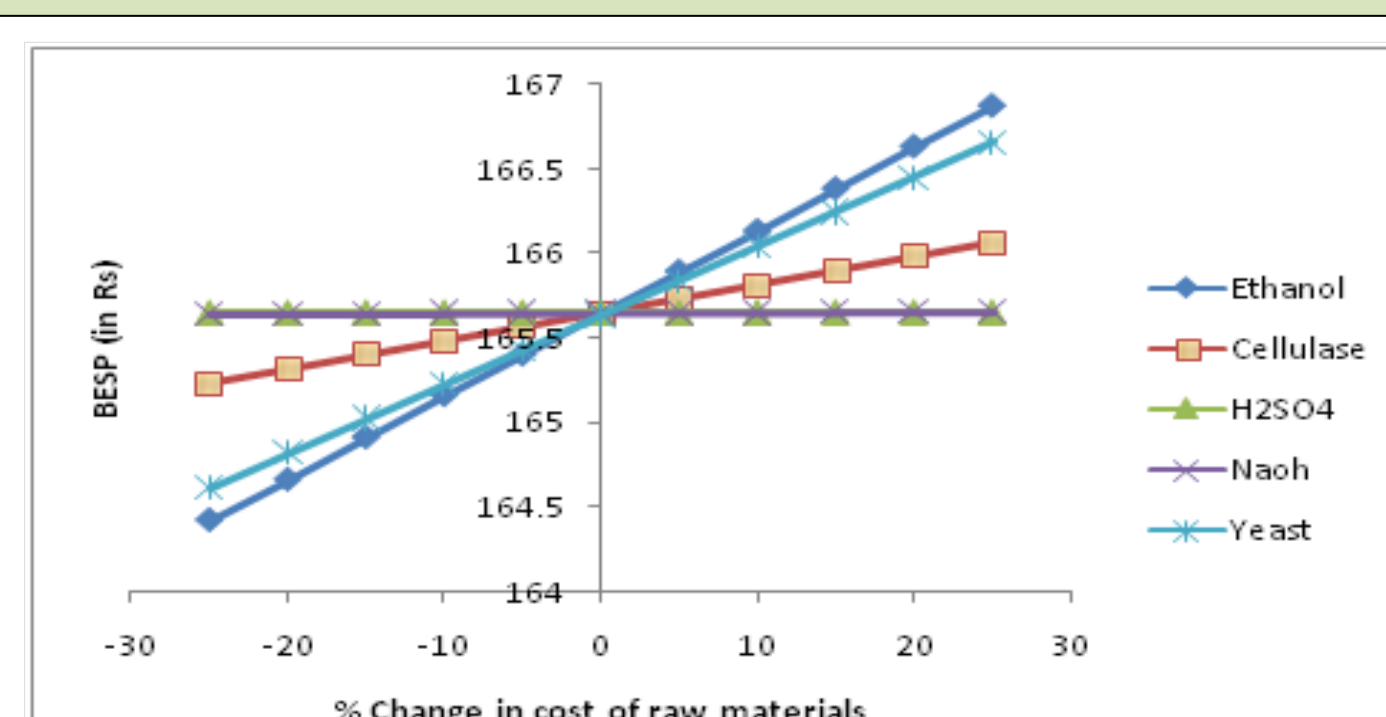
Scenario evaluation & comparison

| Variable | Base Case (With Trash) | Scenario 1 (Without Trash) | Scenario 2 (Not sending lignin to boiler) |
|--------------------------|------------------------|----------------------------|---|
| Bagasse to pre-treatment | 41.89 | 14.88 | 34.91 |
| Bagasse to boiler | 19.33 | 46.35 | 26.32 |
| Lignin to boiler | 11.34 | 4.03 | 0 |
| Lignin to vanillin | 0 | 0 | 0 |
| Trash utilized | 34.84 | 0 | 34.84 |
| Ethanol produced | 32.43 | 16.12 | 28.21 |
| BESP (Rs/litre) | 165.65 | 319.16 | 188.34 |

Sensitivity analysis



2.36% increase in BESP for 5% decrease in trash recovery efficiency



BESP sensitivity order
Ethanol > Yeast > Cellulase > NaOH > H₂SO₄

Conclusions

- Better process integration and resource utilization required.
- Lack of trash utilization causes 64.4 % decrease in bagasse to ethanol production.
- Non-utilization of lignin for heat generation causes 16.6% decrease in bagasse to ethanol production.
- Integration of lignin and trash is essential for ethanol feasibility.
- Sensitivity results indicate more efficient organosolvent recovery required